

Heterogeneous Reactions

key difference for reactants in solid phase:
 fugacity does not depend on pressure, cannot
 change as long as there is any solid present.



$$K(T) = \frac{f_{\text{CaO}} f_{\text{CO}_2}}{f_{\text{CaCO}_3}}$$

$$f_{\text{CaO}} = f_{\text{CaCO}_3} =$$

$$f^\circ = 1 \text{ bar as}$$

long as any $\text{CaO}, \text{CaCO}_3$
 is present

$$\Rightarrow K(T) = y_{\text{CO}_2} \cdot P$$

Example 10.4

Calculate max T for stability of calcite in
 390 ppm CO_2 atmosphere

$$C_p(\text{CaCO}_3) = a + bT - c/T^2 - dT^2 + e\sqrt{T}$$

$$S^\circ(\text{CaCO}_3) = 91.7 \text{ J/mol K} \quad \Delta H^\circ_{\text{form}} = -12076 \frac{\text{kJ}}{\text{mol}}$$

See
Worksheet

→ Illustrate numerical integration of heat capacities,
 van't Hoff Equation ←

$$\Delta H^\circ_{\text{rxn}}(T_2) \approx \Delta H^\circ_{\text{rxn}}(T_1) + \frac{T_2 - T_1}{2} \cdot [\Delta C_p^\circ(T_1) + \Delta C_p^\circ(T_2)]$$

$$\ln[K(T_2)] = \ln[K(T_1)] + \frac{T_2 - T_1}{2} \left[\frac{\Delta H^\circ_{\text{rxn}}(T_1)}{RT_1^2} + \frac{\Delta H^\circ_{\text{rxn}}(T_2)}{RT_2^2} \right]$$

At $T = 298 \text{ K}$

$$\Delta H_{rxn}^{\circ} = 179.0 \text{ kJ/mol}$$

$$\Delta G_{rxn}^{\circ} = 31.2 \frac{\text{kJ}}{\text{mol}} \Rightarrow \ln k = -53$$

$$\text{@ } T = 298 \text{ K}$$

Endothermic reaction: as $T \uparrow$ $k \uparrow$

$$y_{\text{CO}_2} P = 390 \cdot 10^{-6} \cdot 1.01 \text{ bar} = 4.0 \cdot 10^{-4} \text{ bar} = k(T)$$

\Rightarrow $T = 804 \text{ K}$ for $T < 804 \text{ K}$ CaCO_3 stable
 $T > 804 \text{ K}$ CaCO_3 decomposes

Multiple Reactions

Independent reactions $1, 2, \dots, r$

$$k_j(T) = \exp\left(-\frac{\Delta G_{rxn,j}^{\circ}}{RT}\right) \quad j = 1, 2, \dots, r$$

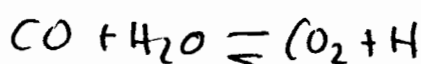
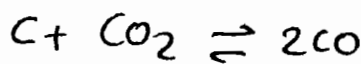
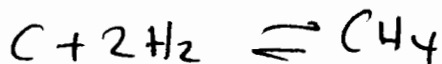
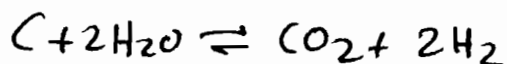
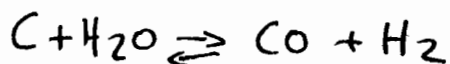
$$f_1^{v_{11}} f_2^{v_{12}} \dots f_n^{v_{1n}} = k_1(T)$$

$$f_1^{v_{21}} f_2^{v_{22}} \dots f_n^{v_{2n}} = k_2(T)$$

$$\vdots$$

$$f_1^{v_{r1}} f_2^{v_{r2}} \dots f_n^{v_{rn}} = k_r(T)$$

Example - Coal Gasification (10.5)

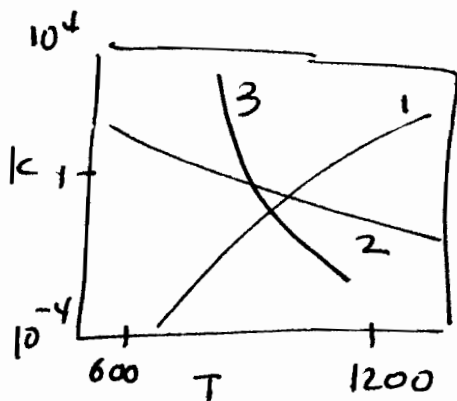
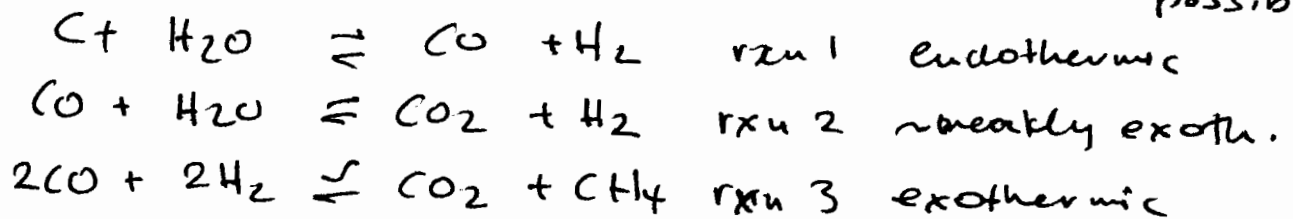


} How many independent reactions?

CBE 246 Heterogeneous Rxn, Multiple Rxn (3)

$$M = \begin{bmatrix} C & H_2O & CO & H_2 & CO_2 & CH_4 \\ -1 & -1 & 1 & 1 & 0 & 0 \\ -1 & -2 & 0 & 2 & 1 & 0 \\ -1 & 0 & 0 & -2 & 0 & 1 \\ -1 & 0 & 2 & 0 & -1 & 0 \\ 0 & -1 & -1 & 1 & 1 & 0 \end{bmatrix} \rightarrow \begin{bmatrix} -1 & -1 & 1 & 1 & 0 & 0 \\ 0 & -1 & -1 & 1 & 1 & 0 \\ 0 & 1 & -1 & -3 & 0 & 1 \\ 0 & 1 & 1 & -1 & -1 & 0 \\ 0 & -1 & -1 & 1 & 1 & 0 \end{bmatrix} \rightarrow \begin{bmatrix} -1 & -1 & 1 & 1 & 0 & 0 \\ 0 & -1 & -1 & 1 & 1 & 0 \\ 0 & 0 & -2 & -2 & 1 & 1 \\ 0 & 0 & 0 & 0 & 0 & 0 \\ 0 & 0 & 0 & 0 & 0 & 0 \end{bmatrix}$$

rank(M) = 3, 3 independent reactions:
 (rows of final matrix - not unique, other choices possible)



Species	Amount
H ₂ O	1 - ξ ₁ - ξ ₂
CO	ξ ₁ - ξ ₂ - 2ξ ₃
H ₂	ξ ₁ + ξ ₂ - 2ξ ₃
CO ₂	ξ ₂ + ξ ₃
CH ₄	ξ ₃
Total	1 + ξ ₁ - 2ξ ₃

$$K_1 = \frac{y_{H_2} y_{CO} P}{y_{H_2O}}$$

$$K_2 = \frac{y_{H_2} y_{CO_2}}{y_{CO} y_{H_2O}}$$

$$K_3 = \frac{y_{CO_2} y_{CH_4}}{y_{CO}^2 y_{H_2}^2}$$

Hard to find ξ₁, ξ₂, ξ₃ initial guesses /
 need solution with constraints:

$$0 \leq y_i \leq 1 \text{ for all species}$$